



Europäisches Patentamt
European Patent Office
Office européen des brevets

① Publication number:

0 399 077
A1



EUROPEAN PATENT APPLICATION

② Application number: 89109427.8

③ Int. Cl. 5: H01M 8/24

② Date of filing: 24.05.89

④ Date of publication of application:
28.11.90 Bulletin 90/48

⑤ Designated Contracting States:
AT BE CH DE ES FR GB GR IT LI LU NL SE

⑦ Applicant: Ishikawajima-Harima Heavy
Industries Co., Ltd.
1-go, 2-ban, 2-chome, Otemachi Chiyoda-ku
Tokyo(JP)

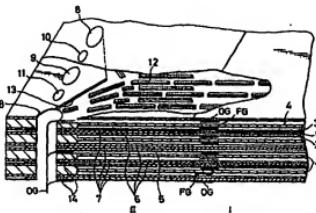
⑦ Inventor: Shiozawa, Shoji
4-23-11, Kita-Terao Tsurumi-ku
Yokohama-shi Kanagawa(JP)
Inventor: Shimizu, Toru
2-3-16, Kami-Kizaki
Urawa-shi Saitama(JP)

⑦ Representative: Schaumburg, Thoenes &
Englaender
Mauerkircherstrasse 31 Postfach 86 07 48
D-8000 München 86 (DE)

⑨ Fuel cell.

⑦ A conventional fuel cell comprises a plurality of cell elements stacked via separator plates (4), each cell element comprising an electrolyte plate (1), a cathode (2) and an anode (3) which sandwich the electrolyte plate (1). A power generation part of the fuel cell is defined by the electrolyte plate (1), cathode (2) and anode (3). Oxidizing gas (OG) and fuel gas (FG) are supplied to each cell element in the same direction but the direction is opposite to the gas flow of an adjacent cell element. In the improvement, preheating devices (11) are provided next to the power generation part (I) as a part of the fuel cell in the direction gases flow in a manner such that both incoming and outgoing gases pass through the preheating device (11). The preheating device (11) includes a plurality of heat exchange promoting elements (12) in the form of projections provided on both faces of the separator plate (4).

FIG.1



EP 0 399 077 A1

Fuel Cell

The present invention relates to a fuel cell that directly converts chemical energy to electrical energy.

Various types of fuel cells are known in the art. Among those, a molten carbonate type fuel cell comprises, as shown in FIGURE 3 of the accompanying drawings, a plurality of fuel cell elements, each of which elements comprises an electrolyte plate (tile) 1, and a cathode electrode (oxide electrode) 2 and an anode electrode (fuel electrode) 3. The tile 1 is a molten carbonate-containing porous plate and is interposed between the cathode and anode electrodes 2 and 3. The fuel cell elements are stacked via separators 4. Oxidizing gas OG is supplied to the cathode electrode 2 and fuel gas FG is supplied to the anode electrode 3, and power generation results from an electrical potential difference between the cathode 2 and the anode electrodes 3.

In the fuel cell, each tile 1, cathode electrode 2, and anode electrode 3 generate heat, respectively. Therefore, in order to secure proper functioning of the fuel cell, it is necessary to maintain the temperature of the tile 1 within a certain range, and to render the temperature distribution of the entire fuel cell as constant as possible.

In the conventional fuel cell, to this end, as shown in FIGURE 4, the oxidizing gas OG and the fuel gas FG are supplied parallel to each other in the same direction in each cell element, while being supplied in the opposite direction relative to the adjacent fuel cell elements. In other words, the fuel gas FG and the oxidizing gas OG that are respectively supplied into one fuel cell along the lower and the upper faces of the tile 1 flow in the same direction (upper two arrows FG and OG in FIGURE 4), while the other pair of fuel gas FG and oxidizing gas OG (lower two arrows FG and OG in FIGURE 4) supplied into the next fuel cell flow in the opposite direction.

The reversal of the gas directions is believed to be effective in suppressing the maximum temperature of the electrolyte 1. However, as depicted in FIGURE 5, the temperature at the exit is still high. In FIGURE 5, a curve A represents the temperature of the cathode gas, B represents that of the anode gas, C represents that of the cell element, the vertical axis indicates the temperature and the horizontal axis indicates a distance ratio from one end of the passage to its other end, i.e., 0 represents the entrance/exit and 1 the exit/entrance. On the other hand, the gas has to be hot at the entrance in order to ensure chemical reactions taking place afterwards. Referring to FIGURE 3, preheated hot gas is supplied to the supply passage in order to

ensure the reaction in the fuel cell element, and accordingly the hot gas is discharged into the discharge passage. High temperature gases make it impossible to use iron pipes in pipings. The fuel cell also requires a preheating device for heating the gas to be supplied to the supply passage. The conventional fuel cell has these defects since heat exchange between a manifold portion of the fuel cell and the electrodes is not considered.

One object of the present invention is to provide a fuel cell which does not require an external preheating device, and in which the gas temperature in the supply passage and the discharge passage are both low as compared with the prior art fuel cell, that results in a simpler design in piping and an improved sealing between the fuel cell and the external pipings thereto.

According to one aspect of the present invention, a fuel cell is provided including a plurality of fuel cell elements of anode electrodes, tiles and cathode electrodes with separator plates being interposed between the fuel cell elements, the cathode gas and the anode gas being supplied in the same direction in one cell element but supplied in the opposite direction in a next cell element, characterized in that preheating devices (also called "preheating part") are provided next to the stack of the fuel cell elements in the width direction of the stack. The preheating device comprises heat exchange promoting elements provided on those parts of the upper and lower faces of each separator that do not face the cathode and anode electrodes. In this specification, the stack of fuel cell elements is called a power generation part of the fuel cell, and the preheating parts are provided at the lateral sides of the power generation part such that the gases supplied/discharged to/from the power generation pass through the preheating parts before they reach/leave the power generation part.

In the fuel cell, the exit of the oxidizing gas of one cell element is formed just next to the entrance of the fuel gas of the adjacent cell element, and the oxidizing gas serves as a cooling gas. Therefore, the oxidizing gas is supplied to a larger amount than the fuel gas. Heat exchange promoting elements are provided on both faces of the separator plates near the entrance and the exit of the gas passages on the separator plates. In each passage, the gas temperature is high at the exit. Therefore, the incoming oxidizing gas of one cell element is heated by the outgoing fuel gas of the next cell element near the entrance of the oxidizing gas passage (or the exit of the fuel gas passage) due to the heat exchange promoting elements. Since the cell elements are stacked, said incoming oxidizing

gas is further heated by the outgoing oxidizing gas via said outgoing fuel gas. When the oxidizing gas is supplied to a large amount, heat exchange mainly takes place between each adjacent two streams of oxidizing gas.

Similarly, near the exit of the oxidizing gas passage of one cell element, heat is transmitted from the hot oxidizing gas to the cold fuel gas via the separator plate, thereby lowering the oxidizing gas temperature while raising the fuel gas temperature. In summary, the gases supplied are heated before they reach the power generation part of the fuel cell, whereas the gases discharged are cooled before they are expelled. Since the temperature of the gases is kept relatively low through the passages, the designing of the fuel cell is simplified, i.e., the piping material does not have to be super-heat resisting material and therefore iron pipes may be used. Since the heat exchange elements are provided within the fuel cell, an external heat exchange device is not required. Furthermore, sealing of the fuel cell is improved because of its temperature.

Now, preferred embodiments of the present invention will be explained with reference to the accompanying drawings.

FIGURE 1 is a sectional view showing a fuel cell according to the present invention.

FIGURE 2 is a graph showing the temperature distribution in the fuel cell according to the present invention;

FIGURE 3 illustrates a sectional view of a fuel cell according prior art;

FIGURE 4 is a graph showing the temperature distribution in the fuel cell according to prior art; and

FIGURE 5 is a graph showing the temperature distribution in the fuel cell of FIGURE 4.

Referring to FIGURE 1, each fuel cell element comprises a plate of electrolyte 1, a cathode electrode 2 and an anode electrode 3. The upper and the lower face of the electrolyte plate 1 are sandwiched by the cathode electrode 2 and the anode electrode 3. The electrolyte plate 1 is a molten carbonate-soaked porous plate in this particular embodiment. A plurality of cell elements are stacked one after another via separator plates 4. Each separator plate 4 has a convex-concave portion or projections on each face thereof. The oxidizing gas OG is supplied to the cathode electrode 2 while the fuel gas FG is supplied to the anode electrode 3. A power generation part of the fuel cell is defined by the electrolyte 1, the cathode 2 and the anode electrode 3. An insulator 5 such as alumina fiber or molten salt is coplanarily provided next to the electrolyte 1 of each cell element. Cover plates 6 and 7 are provided next to the cathode electrode 2 and the anode electrode 3

respectively in the same planes or in the direction the gases flow so that they are coplanar with the cathode and anode electrodes. The cover plates 6 and 7 are fixed on the separators 4 at the convex portion of the separator plate 4. Gas passages 8 and 10, and 9 and 11 for supplying/discharging the oxidizing gas OG and the fuel gas FG, which are called a manifold part, are bored at the periphery of the cover plates 6 and 7. Heat exchange promoting elements 12 are spacedly provided on both faces of the separator plate 4 between the manifold part and the power generation part I in a manner such that the gases are dispersed as they pass therethrough. The heat exchange promoting elements 12 are defined by a plurality of convex elements whose pitch is smaller than the projections of the separator plates 4 which define the gas passages. The convex elements 12 contact the cover plates 6 and 7, so that they also serve as spacer means. Those parts of the fuel cell that the heat exchange promoting elements 12 cover form the preheating part II of the fuel cell. The preheating part II formed on the upper and the lower faces of the separator plates 4 communicate with the corresponding passages respectively via cutouts 13. While the oxidizing gas OG is guided to the cathode 3 of each cell element and discharged from the exit, heat exchange occurs at the entrance and the exit. Numeral 14 designates a packing, such as an asbestos, for the manifold at the periphery of the insulator member 5.

FIGURE 1 illustrates the fuel cell when the oxidizing gas OG is being supplied to the cathode electrode 2. The oxidizing gas supply passage 8 extends vertically and communicates with the passage defined on the upper face of the separator plate due to the cutoff 13. In other words, only the oxidizing gas OG through the passage 8 can flow on the upper face of the separator plate 4.

The oxidizing gas OG and the fuel gas FG flow in parallel to each other and are respectively heated when they pass the power generation part I of the fuel cell. Since the preheating part II are provided at both lateral sides of the fuel cell, sandwiching the power generation part I, heat is exchanged between the high temperature fuel gas FG and the low temperature oxidizing gas at the entrance of the oxidizing gas passage due to a number of heat exchange promoting elements 12 provided on both faces of the separator plates 4 in the preheating part II, even though each pair of oxidizing gas and fuel gas flow in opposite directions in adjacent fuel cell elements. Therefore, the hot outgoing fuel gas FG is cooled in the preheating part II and discharged while the cool incoming gas OG is heated and led to the power generation part I.

At the exit of the oxidizing gas passage, the high temperature oxidizing gas OG is introduced

from the power generation part I into the preheating part II. The low temperature fuel gas flowing next to the oxidizing gas via the separator plate 4 is heated in the preheating part II by heat from the oxidizing gas and led to the power generation part I. The oxidizing gas is thus cooled and discharged.

Temperature distributions in each cell element along the direction the gas flows are shown in FIGURE 2. As seen in a left quarter of FIGURE 2, the incoming cathode gas A is heated by the outgoing anode gas B and further heated by the outgoing cathode gas A in the preheating part II. This shows that the heat exchange between the gases takes place inside the fuel cell. Therefore, the gas to be supplied to the fuel cell is not to be heated beforehand, and lower temperature gas can be supplied to the fuel cell from outside, compared with the conventional fuel cell illustrated in FIGURE 5. The temperature of the outgoing gas is also lower than in the conventional fuel cell. Therefore, the material of the pipes for supplying/discharging does not require high heat resistance. Moreover, a separate preheating device is not required in the gas supply line.

The present invention is not limited to the above embodiments, and various modifications can be made without modifying the idea and the scope of the present invention. For instance, the separator plate 4 may be a corrugated plate or a plate having split type fins. The insulator member 5, too, does not have to be provided.

Claims

1. A fuel cell comprising a plurality of fuel cell elements stacked via separator plates (4), each cell element comprising an electrolyte plate (1), a cathode (2) and an anode (3), the electrolyte plate (1) being sandwiched by the cathode (2) and the anode (3), oxidizing gas (OG) and fuel gas (FG) being supplied to each cell element in the same direction but in the direction opposite to the gas flow of an adjacent cell element, passages for the oxidizing gas (OG) and the fuel gas (FG) being formed by projections provided on both faces of the separator plate (4), and the stack of the cathode (2) and the anode (3) defining a power generation part (I) of the fuel cell, characterized in that preheating devices (II) are provided as a part of the fuel cell next to the power generation part (I) in the direction said gases flow, in a manner such that both incoming and outgoing gases pass through the preheating devices (II) and said preheating devices (II) comprise heat exchange promoting elements (12) provided on both faces of the separator plate (4).

2. A fuel cell according to claim 1, characterized in that said electrolyte plate (1) is a molten

carbonate-soaked porous plate.

3. A fuel cell according to claim 1 or 2, characterized in that said preheating devices (II) are provided at both lateral sides of the power generation part (I), and each of said preheating devices (II) comprises an insulator member (5) and cover plates (6, 7), the insulator member (5) being sandwiched by the cover plates (6, 7), and that the insulator member (5) of each preheating device (II)

10 is coplanarily connected with the electrolyte plate (1).

4. A fuel cell according to any one of the foregoing claims, characterized in that each of said heat exchange promoting elements (12) is an elongated projection provided on each face of the separator plate (4) and arranged in the direction of the gas flow.

5. A fuel cell according to any one of the foregoing claims, characterized in that bores (8, 15 9, 10, 11) which define oxidizing gas passages and fuel gas passages are formed in the preheating parts (II).

6. A fuel cell according to claim 5, characterized in that a plurality of heat exchange promoting elements (12) are provided on both faces of the separator plate (4) between the bores (8, 9, 10, 11) and the power generation part (I), that the pitch of the heat exchange promoting elements (12) is smaller than that of the projections on the separator plate (4), and that the heat exchange promoting elements (12) are spacedly arranged in a manner such that the gases are dispersed.

7. A fuel according to any one of the foregoing claims, characterized in that the heat exchange promoting elements (12) serve as spacer means between the separator plate (4) and the cell element.

40

45

50

55

FIG.1

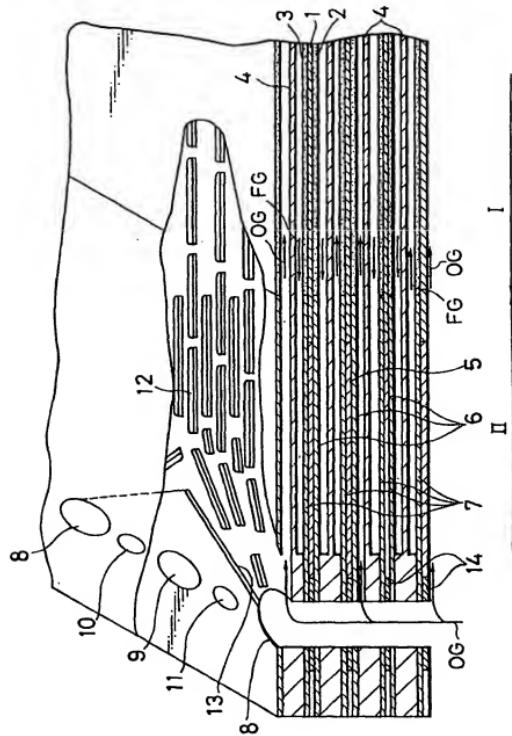


FIG.2

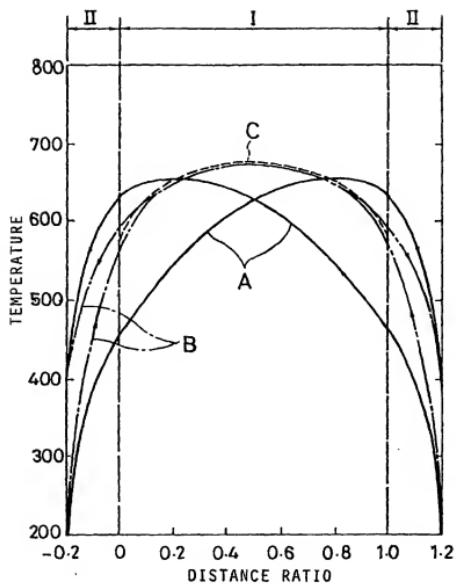


FIG.3

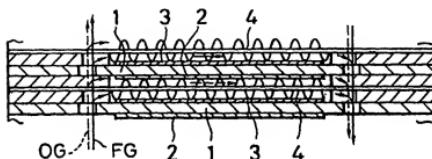


FIG.4

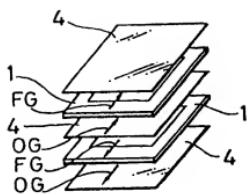
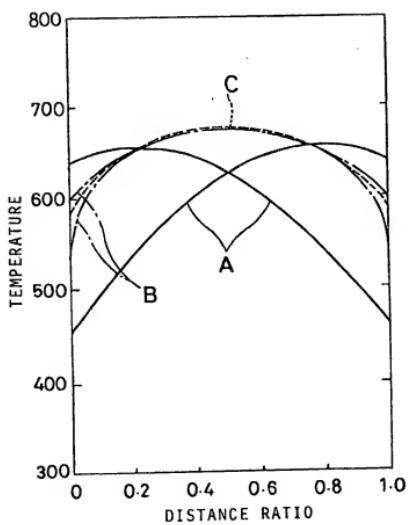


FIG.5





European Patent
Office

EUROPEAN SEARCH REPORT

Application Number

EP 89 10 9427

DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl. 5)
X	JP-A-1 117 278 (ISHIKAWAJIMA HARIMA HEAVY IND. CO., LTD)(10-05-1989) * Abstract * & PATENT ABSTRACTS OF JAPAN, vol. 13, no. 356 (C-803)[3704], 9th August 1989 -----	1-7	H 01 M 8/24
A	US-A-4 708 916 (T. OGAWA et al.) -----		
A	US-A-4 753 857 (M. HOSAKA) -----		
			TECHNICAL FIELDS SEARCHED (Int. Cl. 5)
			H 01 M
The present search report has been drawn up for all claims			
Place of search	Date of completion of the search	Examiner	
THE HAGUE	10-01-1990	D'HONDT J.W.	
CATEGORY OF CITED DOCUMENTS			
X : particularly relevant if taken alone	T : theory or principle underlying the invention		
Y : particularly relevant if combined with another	E : earlier patent document, but published no, or		
Z : particularly relevant if part of the same category	after the filing date		
A : technological background	D : document cited in the application		
O : non-written disclosure	I : document cited for other reasons		
P : intermediate document	& : member of the same patent family, corresponding		
	document		